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This supplemental databook is complementary to the Angeles Link High-Level Economic Analysis and Cost Effectiveness Study prepared by Wood Mackenzie.



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Financial Assumptions

Parameter	Unit	Value	Source
Federal tax rate	%	21.0%	Internal Revenue Service
State tax rate	%	8.8%	State of California
Inflation rate	%	2.0%	Wood Mackenzie
Period of valuation	years	25	Industry Standard
Discount date	dd/mm/yyyy	1/1/2024	SoCalGas
WACC	%	7.67%	SoCalGas WACC from CPUC Resolution E-5306
Depreciation timeframe	years	20	Assumption
Depreciation method	na	Straight Line	
Owners Cost	% of CAPEX	10.0%	
Days in year	Days	365	

Tax Credits

Parameter	Unit	Value	Source
Tax Credits			
H2 production tax credit	US\$/kg-H2, Real 2024	\$3.00	Inflation Reduction Act
H2 production tax credit last start year	year	2033	
H2 production tax credit years	year	10	
Power ITC	%	30.0%	
Power PTC	US\$/kWh, Real 2024	\$0.03	
ITC/PTC last start year	year	2036	
Power PTC years	years	10	
Power Tax credits (ITC/PTC) phase out percentages			
2023-2033	year	100.00%	Inflation Reduction Act
2034-2035	year	75.00%	
2035-2036	year	50.00%	
2036+	year	0.00%	

CAPEX Schedule

Parameter	Unit	Value	Source
CAPEX Schedule			
2025	Start year -5	0.00%	Assumption
2026	Start year -4	0.00%	
2027	Start year -3	0.00%	
2028	Start year -2	75.00%	
2029	Start year -1	25.00%	

Distances Assumptions

Parameter	Unit	Value	Source
Pipeline Route Distances			
San Joaquin Valley Route to Delivery Point	miles	250	Design Study
Palmdale / Lancaster Route to Delivery Point	miles	100	
Blythe Route to Delivery Point	miles	235	
Trucking Routes Distances			
San Joaquin Valley to San Joaquin Valley Depleted Oil Fields Storage	miles	140	Estimated from Design Study Inputs
Palmdale / Lancaster to San Joaquin Valley Depleted Oil Fields Storage	miles	90	
Blythe to Out of State Salt Cavern Storage	miles	100	
San Joaquin Valley Depleted Oil Fields Storage to Distribution Delivery Point	miles	140	
Out of State Salt Cavern Storage to Distribution Delivery Point	miles	335	
Shipping Routes Distances			
Northern California	nm (vessel)	450	Assumption
In-Basin Production with Power T&D Routes Distances			
San Joaquin Valley	miles	300	Estimated from Design Study Inputs
Palmdale / Lancaster	miles	100	
Blythe	miles	235	
Delivery Pipeline Length			
Delivery/Distribution Line	miles	79	Design Study

Upstream Assumptions for Angeles Link & Delivery Alternatives (Except Localized Hub)

Parameter	Unit	Value	Source
Power Feedstock			
H2 power demand	kWh / kg-H2	60	Production Study
Solar capacity factor	%	26.40%	
Water Feedstock			
Water usage intensity	kg H2O per kg H2	14	Water Study
Water cost	US\$/m3	\$2.51	
Hydrogen Production			
Electrolyzer building block	MW	200	Production Study
Stack lifetime (hours)	hours	34,087	
Stack replacement CAPEX	US\$/kW	\$508.82	
Electrolyzer unit cost	US\$/kW	\$2,707.38	
Fixed Electrolyzer O&M (% / yr of capex)	%	0.74%	
Production losses	%	2.00%	Air Studies
Degradation factor	%	0.75%	Wood Mackenzie
Electrolyzer owners cost	%	10.00%	Assumption
Online factor	days	365	

Liquefaction or Methanol Conversion

Parameter	Unit	Value	Source
Hydrogen Liquefaction			
Liquefaction CAPEX per train	US\$ MM	\$124.96	Wood Mackenzie Hydrogen Midstream Model
H2 liquefaction train size	tpd	30	
Liquefaction fixed O&M (% / yr of capex)	%	1.00%	National Petroleum Council
Power consumption	kWh/kgH2	10	
Hydrogen conversion losses	%	0.00%	Assumption
Methanol conversion			
Methanol plant CAPEX	US\$ MM/tpd hydrogen	\$2.49	Wood Mackenzie Hydrogen Midstream Model
Methanol conversion losses	%	0.00%	
Methanol storage time	days	14	
Fixed O&M (% / yr of capex)	%	1.24%	
Methanol storage CAPEX	\$/m3	\$311.06	

Storage

Parameter	Unit	Value	Source
Gaseous Storage			
Total Storage Capacity for Scenario 7	tH2	425,000	Production Study
Total Storage Throughput for Scenario 7	tH2	968,000	
Turnover frequency, nameplate capacity basis for Scenario 7	1/year	2.28	
Storage Capacity per Unit (gaseous)	tH2	5,000	National Petroleum Council
Pressure (gaseous storage)	bar	150	
Tank CAPEX (cH2 Storage)	\$/kgH2	\$17.88	
Compressor CAPEX (cH2 Storage)	\$/kgH2-year	\$0.78	
Fixed O&M (cH2 Storage)	% CAPEX	2.00%	
cH2 Storage power demand	kWh/kgH2	2	
cH2 Storage boil-off rate	% per day	0.00%	
Liquid Storage			
Total Storage Capacity for Scenario 7	tH2	425,000	Production Study
Total Storage Throughput for Scenario 7	tH2	968,000	
Turnover frequency, nameplate capacity basis for Scenario 7	1/year	2.28	
Storage Capacity per unit (Liquid)	tH2	700	National Petroleum Council
Pressure (liquid storage)	bar	<5	
Tank Capex (LH2 Storage)	\$/kgH2	\$41.72	
Liquefier CAPEX (LH2 Storage)	\$/kgH2-year	\$10.58	
Fixed O&M (LH2 Storage)	% CAPEX	2.00%	
LH2 Storage power demand	kWh/kgH2	10	
LH2 Storage boil-off rate	% per day	0.03%	
Underground Storage: Depleted Oil Fields			
Total Storage Capacity for Scenario 7	tH2	425,000	Production Study
Total Storage Throughput for Scenario 7	tH2	968,000	
Turnover frequency, nameplate capacity basis for Scenario 7	1/year	2.28	
Pressure (gaseous storage)	bar	235	Capacity Assessment and Cost Analysis of Geologic Storage of Hydrogen: A Case Study in Intermountain West Region
DOF CAPEX (cH2 Storage)	\$/kgH2	\$2.43	
Fixed O&M (cH2 Storage)	% CAPEX	1.00%	
Compressor CAPEX (cH2 Storage)	\$/kgH2-year	\$0.95	
cH2 Storage power demand	kWh/kgH2	2.20	
Cushion gas percentage from capacity	%	100.00%	
cH2 Storage boil-off rate	% per day	0.00%	
Underground Storage: Salt Caverns			
Total Storage Capacity for Scenario 7	tH2	0	Production Study
Total Storage Throughput for Scenario 7	tH2	N/A	
Turnover frequency, nameplate capacity basis for Scenario 7	1/year	N/A	
Pressure (gaseous storage)	bar	235	Capacity Assessment and Cost Analysis of Geologic Storage of Hydrogen: A Case Study in Intermountain West Region
Salt Cavern CAPEX (cH2 Storage) for Scenario 7	\$/kgH2	N/A	
Fixed O&M (cH2 Storage)	% CAPEX	1.00%	
Compressor CAPEX (cH2 Storage)	\$/kgH2-year	\$0.95	
cH2 Storage power demand	kWh/kgH2	2.20	
Cushion gas percentage from capacity	%	100.00%	
cH2 Storage boil-off rate	% per day	0.00%	

Trucking

Parameter	Unit	Value	Source
Trucks (General)			
Truck speed	Mph	35	Assumption
Shift time	hours per day	8.8	
Truck lifetime	years	12.0	National Petroleum Council
Shifts per day	#	1.0	
Terminal bay lifetime (Trucks)	years	25.0	
Truck fuel consumption	MJ/mi	20.0	
Truck fuel consumption	kgH2/Mi	0.167	
Truck fuel consumption	gal of Diesel/Mi	0.147	
Fuel cost	\$/MJ	0.037	
Gaseous Trucks and Terminal			
Loading bay capacity (gaseous)	tpd	4.0	National Petroleum Council
Capex per bay (gaseous)	US\$ MM	\$11.09	
Fixed O&M gaseous terminal	% of bay CAPEX	5.00%	
Gaseous terminal power demand	kWh/kgH2	3.0	
Gaseous truck CAPEX	US\$ MM	\$1.18	
Fixed O&M gaseous truck	US\$/truck-shift	\$70,627.79	
Non Fuel gaseous truck O&M variable	US\$/mi	\$1.61	
Gaseous truck capacity	kgH2/round trip	1,000	
Gaseous truck loading/unloading losses	%	0.00%	
Gaseous truck unloading losses	%	0.00%	
Gaseous truck boil-off losses	%	2.00%	
Gaseous loading time	hours	1.45	
Gaseous unloading time	hours	1.45	
Liquid Trucks and Terminal			
Loading bay capacity (liquid)	tpd	20.0	National Petroleum Council
Capex per bay (liquid)	US\$ MM	\$105.94	
Fixed O&M liquid terminal	% of bay CAPEX	3.30%	
Liquid terminal power demand	kWh/kgH2	10.0	
Liquid truck CAPEX	US\$ MM	\$1.41	
Fixed O&M liquid truck	US\$/truck	\$188,340.78	
Non Fuel liquid truck O&M variable	US\$/mi	\$1.29	
Liquid truck capacity	kgH2/round trip	4,000	
Liquid truck loading losses	%	0.00%	
Liquid truck unloading losses	%	0.00%	
Liquid truck boil-off losses	%	5.00%	
Liquid loading time	hours	1.45	
Liquid unloading time	hours	1.45	

Shipping

Parameter	Unit	Value	Source	
Shipping (General)				
Fuel price (VLSFO)	\$/tonne	\$595.00	Wood Mackenzie North America Product Markets	
On hire days	days	350.00	Wood Mackenzie Hydrogen Midstream Model	
Fill Rate	%	98.50%		
Shipping Liquid H2				
Vessel size	m3	10,000	Wood Mackenzie Hydrogen Midstream Model	
Vessel speed	knots	19.00		
LH2 boil-off rate	% per day	0.23%		
Port days loading	days	0.75		
Port days discharge	days	0.75		
Port fuel consumption	tpd	4.00		
At sea fuel consumption laden	tpd	45.00		
At sea fuel consumption ballast	tpd	19.00		
Port charge loading/unloading	US\$ MM	\$0.03		
Vessel liquid H2 CAPEX	US\$ MM	\$51.02		
Vessel liquid H2 OPEX	US\$ MM	\$2.27		
Shipping Methanol				
Vessel size	m3	174,000		Wood Mackenzie Hydrogen Midstream Model
Vessel speed	knots	19.00		
Methanol boil-off rate	% per day	0.00%		
Port days loading	days	1.50		
Port days discharge	days	1.50		
Port fuel consumption	tpd	25.00		
At sea fuel consumption laden	tpd	105.00		
At sea fuel consumption ballast	tpd	105.00		
Port charge loading/unloading	US\$ MM	\$0.20		
Vessel liquid methanol CAPEX	US\$ MM	\$217.77		
Vessel liquid methanol OPEX	US\$ MM	\$4.13		

H2 Regasification and Methanol Reconversion

Parameter	Unit	Value	Source
H2 Regasification			
Regasifier CAPEX	\$/Nm3/h	\$956.38	Wood Mackenzie Hydrogen Midstream Model
Regas power consumption	kW/Nm3/h	0.05	
Fixed O&M H2 regas (% / yr of capex)	%	1.24%	
Hydrogen regas losses	%	0.00%	
Liquid hydrogen storage CAPEX	\$/m3	\$4,251.11	
Hydrogen storage time	days	4.00	
Methanol Reconversion			
Methanol reformer CAPEX	US\$ MM/tpd hydrogen	\$6.08	Wood Mackenzie Hydrogen Midstream Model
Methanol boil off	%/day	0.01%	
Methanol storage CAPEX	\$/m3	\$311.06	
Methanol storage time	days	14.00	
Methanol reconversion losses	%	0.00%	
Fixed O&M (% / yr of capex)	%	0.90%	
LP hydrogen storage CAPEX	\$/kgH2	\$680.63	
Hydrogen storage time	days	0.00	



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Production by Scenario

Parameter	Unit	Scenario 1	Scenario 2	Scenario 3	Scenario 4	Scenario 5	Scenario 6	Scenario 7	Scenario 8	Comments
Total Production	Mbps	0.5	0.5	0.5	1	1	1	1.5	1.5	Total project size (Mbps)

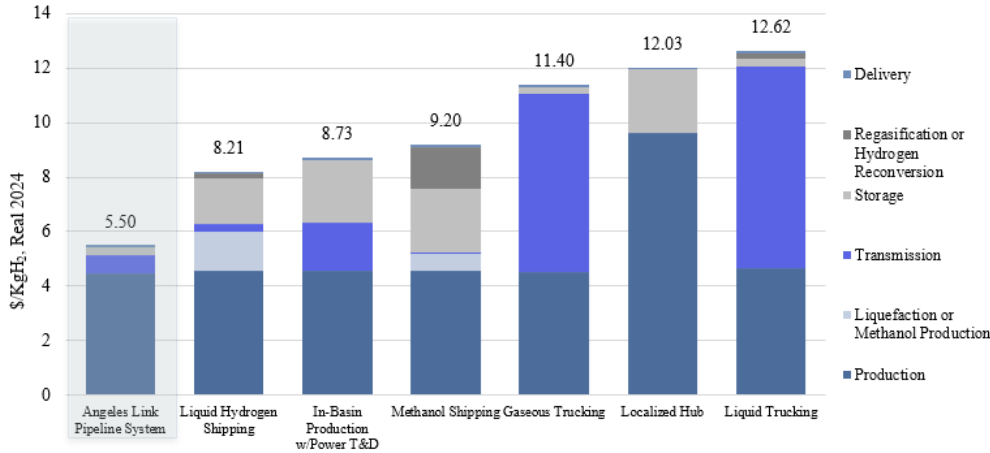
Volume Allocation by Corridor

Parameter	From	To	Scenario 1	Scenario 2	Scenario 3	Scenario 4	Scenario 5	Scenario 6	Scenario 7	Scenario 8	Comments
Allocation of volumes by Production Location											
Production %	From	San Joaquin Valley	100.0%				50.0%	50.0%	50.0%	33.3%	Split from production locations
Production %	From	Palmdale / Lancaster		100.0%			50.0%	50.0%	50.0%	33.3%	Split from production locations
Production %	From	Blythe			100.0%		50.0%	50.0%	50.0%	33.3%	Split from production locations
% of Average Supply Delivered to Storage vs. LA Basin											
Average	To LA Basin	San Joaquin Valley	36.8%			0.0%		34.3%	0.0%	0.0%	Assumption % of avg prod to destination
Average	To LA Basin	Palmdale / Lancaster		36.8%		68.6%	34.3%		70.9%	70.9%	Assumption % of avg prod to destination
Average	To LA Basin	Blythe			36.8%		34.3%			35.5%	Assumption % of avg prod to destination
Average	To Storage	San Joaquin Valley to SJV	63.2%	0.0%	0.0%	100.0%	0.0%	65.7%	100.0%	100.0%	Assumption % of avg prod to destination
Average	To Storage	Palmdale / Lancaster to SJV	0.0%	63.2%	0.0%	31.4%	65.7%	0.0%	29.1%	29.1%	Assumption % of avg prod to destination
Average	To Storage	Blythe to OOS	0.0%	0.0%	63.2%	0.0%	65.7%	65.7%	0.0%	64.5%	Assumption % of avg prod to destination
Average	In/out Storage	SJV Depleted Oil Field Storage to Port	63.2%	63.2%	0.0%	131.4%	65.7%	65.7%	129.1%	129.1%	Total avg flow into storage
Average	In/out Storage	OOS Salt Cavern Storage to Port	0.0%	0.0%	63.2%	0.0%	65.7%	65.7%	0.0%	64.5%	Total avg flow into storage
% of Maximum Supply Delivered to Storage vs. LA Basin											
Max	To LA Basin	San Joaquin Valley	43.3%			0.0%		34.2%	0.0%	0.0%	Assumption % of max prod to destination
Max	To LA Basin	Palmdale / Lancaster		43.3%		68.4%	34.2%		76.7%	76.7%	Assumption % of max prod to destination
Max	To LA Basin	Blythe			43.3%		34.2%			38.4%	Assumption % of max prod to destination
Max	To Storage	San Joaquin Valley to SJV	56.7%	0.0%	0.0%	100.0%	0.0%	65.8%	100.0%	100.0%	Assumption % of max prod to destination
Max	To Storage	Palmdale / Lancaster to SJV	0.0%	56.7%	0.0%	31.6%	65.8%	0.0%	23.3%	23.3%	Assumption % of max prod to destination
Max	To Storage	Blythe to OOS	0.0%	0.0%	56.7%	0.0%	65.8%	65.8%	0.0%	61.6%	Assumption % of max prod to destination
Max	In/out Storage	SJV Depleted Oil Field Storage to Port	56.7%	56.7%	0.0%	113.0%	65.8%	65.8%	123.3%	123.3%	Total max flow into storage
Max	In/out Storage	OOS Salt Cavern Storage to Port	0.0%	0.0%	56.7%	0.0%	65.8%	65.8%	0.0%	61.6%	Total max flow into storage
Ratio of Average to Maximum Flows by Corridor											
Ratio avg to max	Production	San Joaquin Valley	1.44			1.44		1.44	1.44	1.44	Max flow prod / avg flow prod
Ratio avg to max	Production	Palmdale / Lancaster		1.44		1.44	1.44		1.44	1.44	Max flow prod / avg flow prod
Ratio avg to max	Production	Blythe			1.44		1.44	1.44		1.44	Max flow prod / avg flow prod
Ratio avg to max	To Storage	SJV Depleted Oil Field Storage to Port	0.00	0.00	0.00	0.00	0.00	0.00	0.00	1.77	Max flow into storage / avg flow prod
Ratio avg to max	To Storage	OOS Salt Cavern Storage to Port	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.89	Max flow into storage / avg flow prod
Ratio avg to max	To LA Basin	SJV Depleted Oil Field Storage to Port	1.77	1.77		4.26	2.13	2.13	3.88	4.11	Max flow out / avg flow prod
Ratio avg to max	To LA Basin	OOS Salt Cavern Storage to Port			1.77		2.13	2.13		1.71	Max flow out / avg flow prod

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Notes: Reflects costs from Scenario 7 for 1.5 Mtpa. Production is assumed to begin in 2030 to take advantage of tax incentives, including Production Tax Credits (PTC) for hydrogen (45V)⁶⁶ and power (45Y),⁶⁷ which provide up to \$3 per kgH₂ and \$0.028 per kWh for ten years. Storage assumptions were based on proximity to production sites, and the geographic footprint under consideration for storage in the Production Study.⁶⁸ For Angeles Link and the trucking alternatives (gaseous and liquid), identified routes allowed for access to underground storage sites, therefore, underground storage costs were assumed. Delivery alternatives with production sites that did not overlap with the identified geological storage sites, were assumed to rely on above ground storage. These alternatives include shipping, in-basin production with T&D, and localized hub. The shipping solutions include the costs of specialized handling required to deliver methanol and liquid hydrogen. The cost for liquefaction in the liquid hydrogen trucking alternative is included as a part of transmission costs.



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Mobility Input Assumptions

Class 8 Sleeper Cab					Transit Bus				
Assumptions	Low	Base	High	Sources	Assumptions	Low	Base	High	Sources
Fuel economy (MPGe)					Fuel economy (MPGe)				
FCEV		13		Argonne National Laboratory	FCEV		17		Argonne National Laboratory
BEV		23			BEV		29		
Tank range (mi):					Tank range (mi):				
FCEV		420		Representative vehicle specifications from OEMs	FCEV		370		Representative vehicle specifications from OEMs
BEV		275			BEV		300		
Purchase cost (\$k):					Purchase cost (\$k):				
FCEV		\$228	\$456	Argonne National Laboratory	FCEV		\$311	\$623	Argonne National Laboratory
BEV		\$255	\$510		BEV		\$311	\$623	
Labor cost (\$/mi)		\$0.94			Labor cost (\$/mi)		\$0.94		
Dwell cost (\$/hr)		\$89		Dwell cost (\$/hr)		\$89			
Refueling rate (mins):					Refueling rate (mins):				
FCEV		10	30	Argonne National Laboratory	FCEV		10	30	Argonne National Laboratory
BEV		20	60	Argonne National Laboratory and Wood Mackenzie TCO Model	BEV		20	60	Argonne National Laboratory and Wood Mackenzie TCO Model
Fuel cost (net of applicable LCFS)					Fuel cost (net of applicable LCFS)				
FCEV (\$/kg)	\$4.51	\$6.01	\$7.51	Includes the LCOH from Angeles Link of \$5.29 + \$1.85 distribution cost + \$0.70 dispensing cost - \$2.04 LCFS credit pass through Assuming a SCE EV charging tariff and applying a retail projection along with a retail markup. Assuming LCFS credits are included in the retail markup	FCEV (\$/kg)	\$4.51	\$6.01	\$7.51	Includes the LCOH from Angeles Link of \$5.29 + \$1.85 distribution cost + \$0.70 dispensing cost - \$2.04 LCFS credit pass through Assuming a SCE EV charging tariff and applying a retail projection along with a retail markup. Assuming LCFS credits are included in the retail markup
BEV (\$/kWh)	\$0.31	\$0.43	\$0.60		BEV (\$/kWh)	\$0.31	\$0.43	\$0.60	

Class 8 Drayage					Class 8 Day Cab				
Assumptions	Low	Base	High	Sources	Assumptions	Low	Base	High	Sources
Fuel economy (MPGe)					Fuel economy (MPGe)				
FCEV		12		Argonne National Laboratory	FCEV		13		Argonne National Laboratory
BEV		22			BEV		23		
Tank range (mi):					Tank range (mi):				
FCEV		450		Representative vehicle specifications from OEMs	FCEV		500		Representative vehicle specifications from OEMs
BEV		200			BEV		300		
Purchase cost (\$k):					Purchase cost (\$k):				
FCEV		\$185	\$371	Argonne National Laboratory	FCEV		\$201	\$402	Argonne National Laboratory
BEV		\$166	\$331		BEV		\$187	\$373	
Labor cost (\$/mi)		\$0.94			Labor cost (\$/mi)		\$0.94		
Dwell cost (\$/hr)		\$89		Dwell cost (\$/hr)		\$89			
Refueling rate (mins):					Refueling rate (mins):				
FCEV		10	30	Argonne National Laboratory	FCEV		10	30	Argonne National Laboratory
BEV		20	60	Argonne National Laboratory and Wood Mackenzie TCO Model	BEV		20	60	Argonne National Laboratory and Wood Mackenzie TCO Model
Fuel cost (net of applicable LCFS)					Fuel cost (net of applicable LCFS)				
FCEV (\$/kg)	\$4.51	\$6.01	\$7.51	Includes the LCOH from Angeles Link of \$5.29 + \$1.85 distribution cost + \$0.70 dispensing cost - \$2.04 LCFS credit pass through Assuming a SCE EV charging tariff and applying a retail projection along with a retail markup. Assuming LCFS credits are included in the retail markup	FCEV (\$/kg)	\$4.51	\$6.01	\$7.51	Includes the LCOH from Angeles Link of \$5.29 + \$1.85 distribution cost + \$0.70 dispensing cost - \$2.04 LCFS credit pass through Assuming a SCE EV charging tariff and applying a retail projection along with a retail markup. Assuming LCFS credits are included in the retail markup
BEV (\$/kWh)	\$0.34	\$0.35	\$0.49		BEV (\$/kWh)	\$0.34	\$0.35	\$0.49	



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Power Input Assumptions

x **Hydrogen Combustion Turbine Retrofit**

Assumptions	Low	Base	High	Sources
Facility size (MW)	500			Wood Mackenzie LCOE Model
Net capacity factor (%)				
Baseload	60%	50%	40%	Wood Mackenzie LCOE Model
Peaking	11%	10%	9%	
Capex (\$/kW)				
Baseload – retrofit	\$156	\$208	\$260	NPC Study
Peaking – retrofit	\$156	\$208	\$260	
Fixed O&M (\$/kW-yr)				
Baseload	\$70	\$78	\$86	Wood Mackenzie LCOE Model
Peaking	\$51	\$56	\$62	
Variable O&M (\$/MWh)				
Baseload	\$3	\$4	\$4	Wood Mackenzie LCOE Model
Peaking	\$11	\$13	\$14	
Fuel cost				
Angeles Link LCOH (\$/kg)	\$4.13	\$5.50	\$6.88	Cost Effectiveness Study LCOH
Energy equivalent (\$/MMBtu _e)	\$31	\$41	\$51	Conversion of LCOH to energy equivalent in MMBtu

x **Battery Storage Facility - 12 hour**

Assumptions	Low	Base	High	Sources
Facility size (MW)	400			Based on Moss Landing, largest operating facility in California
Discharge duration (Hours)	12			Wood Mackenzie LCOE Model
Roundtrip efficiency (%)	86%			
Net capacity factor (%)	12%	10%	8%	Follows from duration and assumes 30+ cycles per year
Capex (\$/kW)	\$2,526	\$3,367	\$4,209	Wood Mackenzie LCOE Model
Fixed O&M (\$/kW-yr)	\$95	\$119	\$143	
Variable O&M (\$/MWh)	\$10	\$13	\$16	
Charging cost (\$/MWh)	\$44	\$59	\$71	Forecast of average annual wholesale price forecast for CAISO SP15
ITC (%)	30%			Forecast reflecting outlook on current policy

x **Gas Turbine with CCS Retrofit**

Assumptions	Low	Base	High	Sources
Facility size (MW)	500			Wood Mackenzie LCOE Model
Net capacity factor (%)	60%	50%	40%	
Capex (\$/kW)				
Baseload - retrofit	\$1,243	\$1,775	\$2,308	Wood Mackenzie LCOE Model
Fixed O&M (\$/kW-year)	\$64	\$91	\$119	Wood Mackenzie LCOE Model
Variable O&M (\$/MWh)	\$4	\$5	\$7	
Fuel cost				
Delivered fuel cost (\$/MMBtu _e)	\$3.6	\$4.5	\$5.4	Forecast of delivered gas price at SoCalGas Citygate
T&D adder (\$/MMBtu)	\$3.5			Wood Mackenzie LCOE Model
CO ₂ transport and sequestration (\$/ton)	\$92		\$368	Wood Mackenzie CCS Model (California-specific)
45Q credit value (\$/MWh)	\$18			Forecast reflecting outlook on current policy



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Cogeneration Input Assumptions

x

Hydrogen Turbine Retrofit				
Assumptions	Low	Base	High	Sources
Facility size (MW)	30			Wood Mackenzie LCOE Model
Net capacity factor (%)	69	58	46	
Capex (\$/kW)	\$266	\$380	\$494	
Fixed O&M (\$/kW-year)	\$105	\$117	\$129	
Variable O&M (\$/MWh)	\$8	\$9	\$9	
Fuel cost				
Angeles Link LCOH (\$/kg)	\$4.13	\$5.50	\$6.88	Angeles Link LCOH
Energy equivalent (\$/MMBtu _e)	\$31	\$41	\$51	Conversion of LCOH to energy equivalent in MMBtu

x

Gas Turbine with CCS Retrofit				
Assumptions	Low	Base	High	Sources
Facility size (MW)	30			Wood Mackenzie LCOE Model
Net capacity factor (%)	69	58	46	
Capex (\$/kW)	\$2,100	\$3,000	\$3,900	
Fixed O&M (\$/kW-year)	\$124	\$137	\$151	
Variable O&M (\$/MWh)	\$10	\$11	\$13	
Fuel cost				
Delivered fuel cost (\$/MMBtu _e)	\$3.6	\$4.5	\$5.4	Forecast of delivered gas price at SoCal Citygate
T&D adder (\$/MMBtu)	\$3.5			Wood Mackenzie North America Gas Model
CO ₂ transport and sequestration (\$/ton)	\$92		\$368	Wood Mackenzie CCS Model (California-specific)
45Q credit value (\$/MWh)	\$18			Forecast reflecting outlook on current policy

Food & Beverage Input Assumptions

x

Food & Beverage Alternatives

Assumptions	Low	Base	High	Sources
Hydrogen				
Delivered fuel cost (\$/kg)	\$4.1	\$5.5	\$6.9	Angeles Link LCOH
Electricity				
Retail cost (\$/MWh)	\$180	\$225	\$270	SCE Industrial Service Tariffs and Third-Party Forecasts
Green premium - CA REC prices (\$/MWh)	\$25			Wood Mackenzie Long Term Power Model

Cement Input Assumptions

x

Cement Alternatives

Assumptions	Low	Base	High	Sources
Hydrogen				
Delivered fuel cost (\$/kg)	\$4.1	\$5.5	\$6.9	Angeles Link LCOH
Gas + CCS				
Delivered fuel cost (\$/MMBtu)	\$3.6	\$4.5	\$5.4	Wood Mackenzie North America Gas and CCS Models
T&D adder (\$/MMBtu)	\$3.5			
CO2 transport and sequestration cost (\$/ton)	\$92		\$368	
Electricity				
Retail cost (\$/MWh)	\$180	\$225	\$270	SCE Industrial Service Tariffs and Third-Party Forecasts
CA REC prices (\$/MWh)	\$25			Wood Mackenzie Long Term Power Model

Refineries Input Assumptions

x

Refinery Alternatives

Assumptions	Low	Base	High	Sources
Clean Renewable Hydrogen				
Delivered feedstock cost (\$/kg)	\$4.1	\$5.5	\$6.9	Angeles Link LCOH
Hydrogen Abated with CCS				
Delivered feedstock cost (\$/kg)	\$1.8		\$3.5	Wood Mackenzie LCOH Model
CO ₂ transport and sequestration cost (\$/ton)	\$92		\$368	Wood Mackenzie CCS Models (California-specific)

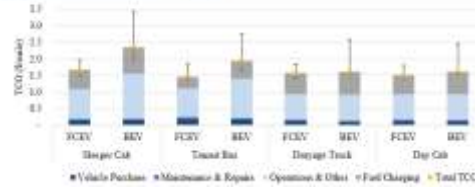
Note: The output tables shown below were used to generate the charts in the Cost Effectiveness Report. A screenshot of the corresponding chart has been provided.

Mobility

x TCO Cost Effectiveness - Mobility

	Sleeper Cab		Transit Bus		Drayage Truck		Day Cab	
	FCEV	BEV	FCEV	BEV	FCEV	BEV	FCEV	BEV
Vehicle Purchase	\$0.15	\$0.17	\$0.19	\$0.19	\$0.12	\$0.11	\$0.13	\$0.12
Maintenance & Repairs	\$0.04	\$0.02	\$0.05	\$0.02	\$0.04	\$0.02	\$0.04	\$0.02
Operations & Other	\$0.90	\$1.36	\$0.88	\$1.20	\$0.77	\$0.79	\$0.76	\$0.80
Fuel/Charging	\$0.59	\$0.81	\$0.35	\$0.53	\$0.64	\$0.70	\$0.59	\$0.67
TCO - Base	\$1.68	\$2.36	\$1.47	\$1.94	\$1.57	\$1.62	\$1.52	\$1.61
TCO - High	\$1.99	\$3.43	\$1.86	\$2.76	\$1.84	\$2.59	\$1.80	\$2.46
TCO - Low	\$1.47	\$1.94	\$1.33	\$1.64	\$1.43	\$1.52	\$1.39	\$1.52

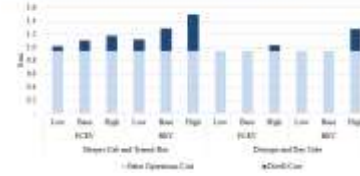
Figure 7: Cost Effectiveness: Mobility (2030)¹



x Dwell Cost Proportion of Operations Cost

	Sleeper Cab and Transit Bus						Drayage and Day Cabs					
	FCEV			BEV			FCEV			BEV		
	Low	Base	High	Low	Base	High	Low	Base	High	Low	Base	High
Other Operations Cost	\$0.94	\$0.94	\$0.94	\$0.94	\$0.94	\$0.94	\$0.94	\$0.94	\$0.94	\$0.94	\$0.94	\$0.94
Dwell Cost	\$0.08	\$0.16	\$0.24	\$0.18	\$0.35	\$0.56	\$0.00	\$0.00	\$0.00	\$0.00	\$0.00	\$0.34

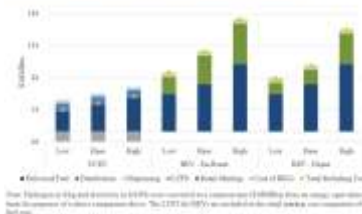
Figure 8: Dwell Cost Proportion of Total Operations Costs Across Technologies¹



x Fuel/Charging Cost Breakdown

	FCEV			BEV - En-Route			BEV - Depot		
	Low	Base	High	Low	Base	High	Low	Base	High
Delivered Fuel	\$30.69	\$40.92	\$51.15	\$58.31	\$73.84	\$104.89	\$58.31	\$73.84	\$104.89
Distribution	\$13.76	\$13.76	\$13.76						
Dispensing	\$5.21	\$5.21	\$5.21						
LCFS	-\$15.18	-\$15.18	-\$15.18						
Retail Markup				\$26.24	\$44.30	\$62.94	\$17.49	\$22.15	\$47.20
Cost of RECs				\$7.44	\$7.44	\$7.44	\$7.44	\$7.44	\$7.44
Total Refueling Cost	\$34.49	\$44.72	\$54.95	\$91.99	\$125.58	\$175.27	\$83.24	\$103.43	\$159.54

Figure 9: Fuel/Charging Cost Breakdown by Technology and Refueling Point¹



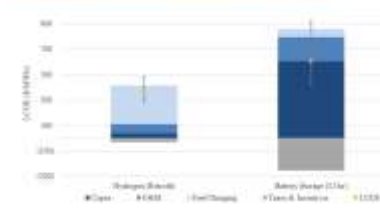
Power and Cogeneration Outputs

Hydrogen vs Electrification

x LCOE Cost Effectiveness - Power

	Hydrogen (Retrofit)	Battery Storage (12-hr)
Capex	\$38	\$606
O&M	\$73	\$189
Fuel/Charging	\$303	\$67
Taxes & Incentives	-\$30	-\$252
LCOE - Base	\$384	\$609
LCOE - High	\$483	\$923
LCOE - Low	\$288	\$419

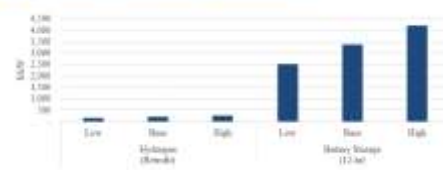
Figure 10: Cost Effectiveness: Power (Hydrogen and Battery Storage) (2024)



x Capital Cost

	Hydrogen (Retrofit)			Battery - 12 hr		
	Low	Base	High	Low	Base	High
Capital Expenditures	\$156	\$208	\$260	\$2,526	\$3,367	\$4,209

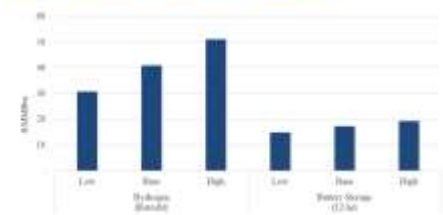
Figure 11: Capital Cost of Hydrogen Turbine vs. Battery Storage²⁰²⁴



x Fuel/Charging Cost Breakdown

	Hydrogen (Retrofit)			Battery - 12 hr		
	Low	Base	High	Low	Base	High
Fuel/Charging Expenditure	\$31	\$41	\$51	\$15	\$17	\$19

Figure 12: Fuel/Charging Cost of Hydrogen Turbine vs. Battery Storage²⁰²⁴



Hydrogen vs CCS

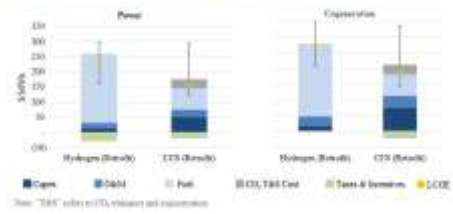
x LCOE Breakdown - Power

	Hydrogen (Retrofit)	CCS (Retrofit)
Capex	\$12	\$50
O&M	\$19	\$25
Fuel/Charging	\$227	\$70
CO2 T&S Cost	\$0	\$31
Taxes & Incentives	-\$30	-\$19
LCOE - Base	\$229	\$157
LCOE - High	\$298	\$294
LCOE - Low	\$164	\$120

LCOE Breakdown - Cogeneration

	Hydrogen (Retrofit)	CCS (Retrofit)
Capex	\$16	\$74
O&M	\$31	\$40
Fuel/Charging	\$227	\$67
CO2 T&S Cost	\$0	\$30
Taxes & Incentives	\$2	-\$23
LCOE - Base	\$277	\$189
LCOE - High	\$351	\$333
LCOE - Low	\$208	\$144

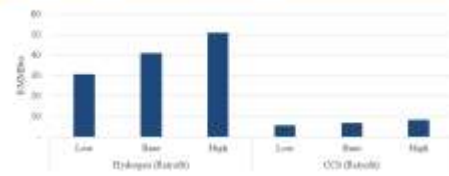
Figure 14: Cost Effectiveness: Power & Cogeneration (Hydrogen and CCS) (2020)



x Fuel Cost Variation

	Hydrogen (Retrofit)			CCS (Retrofit)		
	Low	Base	High	Low	Base	High
Fuel Cost	\$30.7	\$40.9	\$51.2	\$6.4	\$8.0	\$9.5

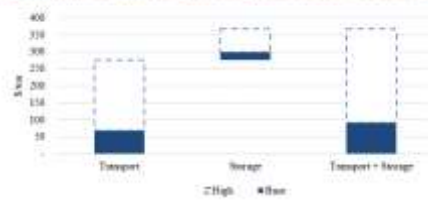
Figure 15: Fuel Cost Variation Across Hydrogen and CCS Alternatives in Power and Cogeneration



x CO2 transport and Storage Cost Sensitivities

	Transport	Storage	Transport + Storage
Base	\$ 69	\$ 23	\$ 92
High	\$ 207	\$ 69	\$ 276

Figure 16: Variations in CO2 Transport and Segregation Costs for CCS Facilities (2020)



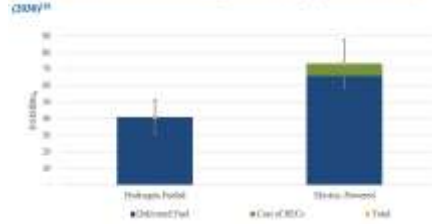
Hydrogen vs Electrification

Industry - Food & Beverage and Cement Outputs

x Cost Effectiveness - F&B and Cement

	Hydrogen-Fueled	Electric-Powered
Delivered Fuel	\$40.9	\$65.9
Cost of RECs	\$0.0	\$7.3
Total - Base	\$40.9	\$73.2
Total - High	\$51.2	\$88.0
Total - Low	\$30.7	\$58.7

Figure 13: Cost Effectiveness: Food & Beverage and Cement (Hydrogen and Electrification)



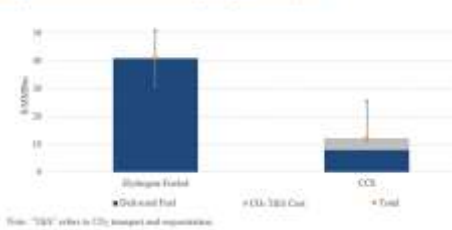
Hydrogen vs CCS

Industry - Cement Outputs

x Cost Effectiveness - Cement

	Hydrogen-Fueled	CCS
Delivered Fuel	\$40.9	\$8.0
CO ₂ T&S Cost	\$0.0	\$4.2
Total - Base	\$40.9	\$12.2
Total - High	\$51.2	\$25.8
Total - Low	\$30.7	\$11.3

Figure 17: Cost Effectiveness: Cement (Hydrogen and CCS) (200t)



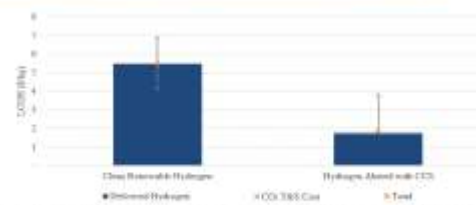
Note: "T&S" refers to CO₂ transport and sequestration.

Industry - Refineries Outputs

x Cost Effectiveness - Refineries

	Clean Renewable Hydrogen	Hydrogen Abated with CCS
Delivered Hydrogen	\$5.5	\$1.7
CO ₂ T&S Cost	\$0.0	\$0.1
Total - Base	\$5.5	\$1.8
Total - High	\$6.9	\$3.8
Total - Low	\$4.1	\$1.8

Figure 18: Cost Effectiveness: Refineries (Clean Renewable Hydrogen and CCS) (100t)



Note: "T&S" refers to CO₂ transport and sequestration. Delivered Hydrogen for the CCS scenario includes the cost of capture equipment.